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# Microchannel Flow of SC-CO<sub>2</sub>+H<sub>2</sub>O system for SEE Process Design



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# The Research Group



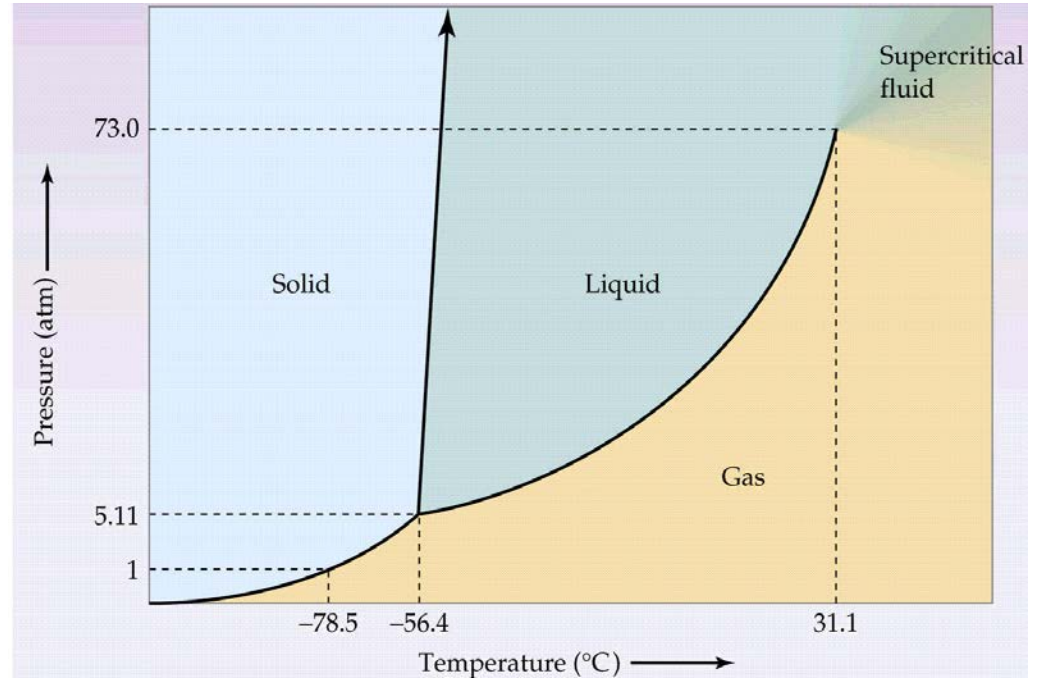
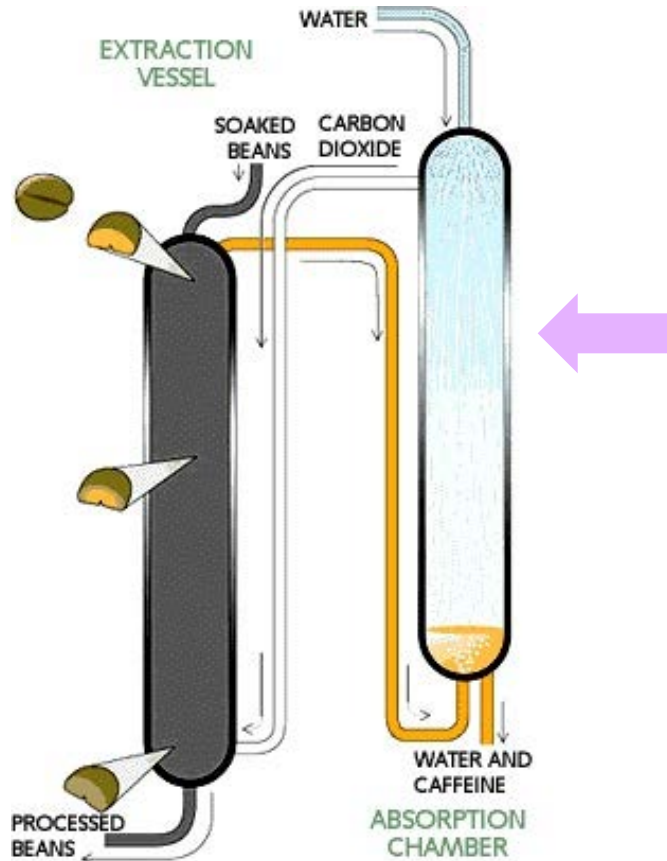
Academic Advisor  
Assoc. Prof.  
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Tutor  
Mr.  
Seiji SHINODA



Group Photo

# 1. Background



Phase diagram of CO<sub>2</sub>

SC-CO<sub>2</sub> Extraction

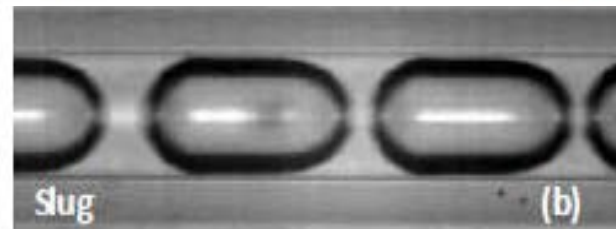
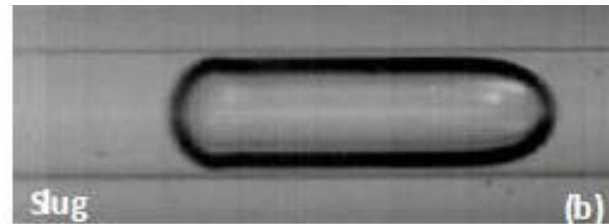
for de-caffeine process ↑

<http://www.beannorth.com/our-beans/the-quality/decaffeination-process/>

Slug Flow

in a microchannel →

<http://www2.egr.uh.edu/~dli9/research.htm>



NEW  
PROCESS  
DESIGN

DESIGN

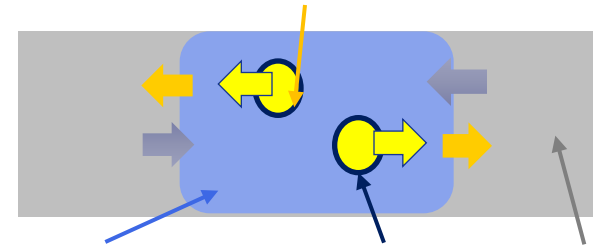
## Nanoparticle System

- Mean diameter between 100 nm and 500 nm, SD/Mean < 0.1 (monodispersion).
- Biomedical use – drug release, drug targeting, injectable scaffolds.

## Supercritical Emulsion Extraction (SEE)

- Fast extraction preventing *aggregation*.

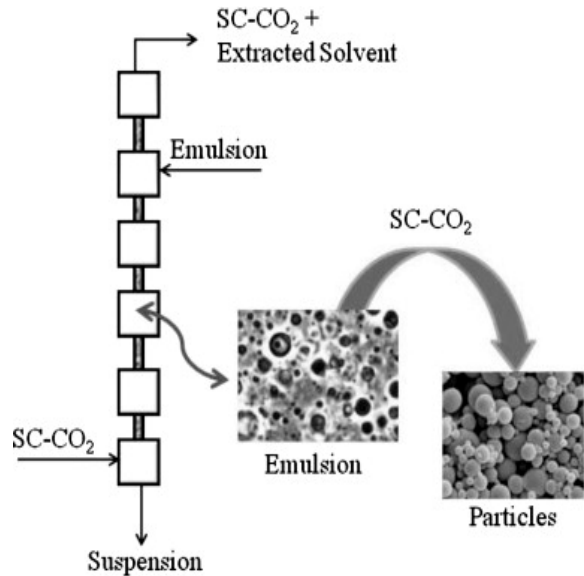
Oil phase (polymer dissolved)



Water phase surfactant SC-CO<sub>2</sub>

Principle of SEE

Adapted from a ppt of Mr. Seiji Shinoda



Previous Work

## Continuous SEE Process

G. D. Porta et al.

J of Supercritical Fluids, 76 (2013): 67-73.

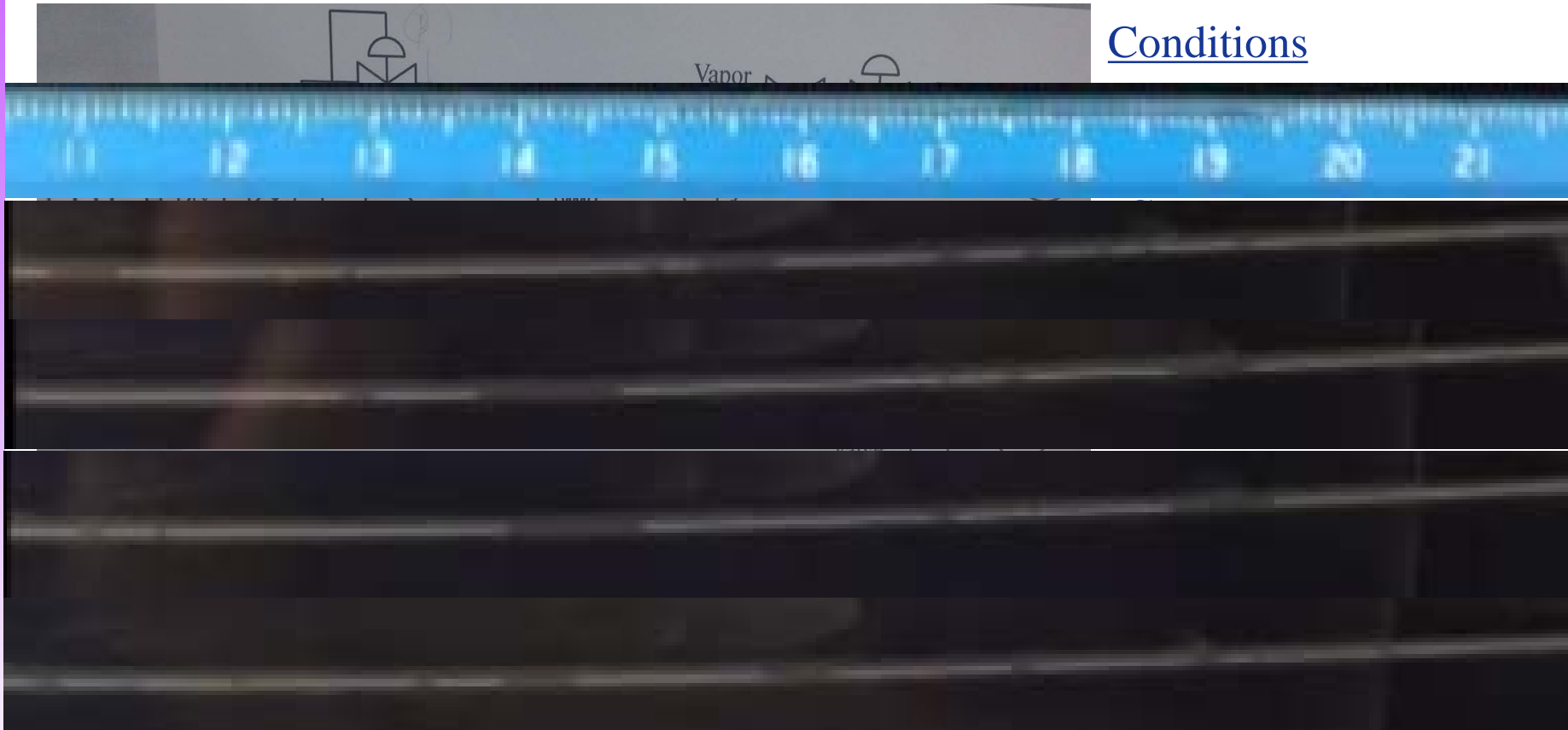
**Aim of the process** – to prepare monodispersed *nanoparticles* by means of *supercritical emulsion extraction* (SEE) in a *microchannel*.

**Purpose of this research** – to study the effect of *liquid/gas ratio* & *temperature* over *slug length*, using SC-CO<sub>2</sub>+H<sub>2</sub>O as a *simulation* system.

→ → mass transfer in the process.



## 2. Method



slugs, calculate the mean.



Electronic balance.

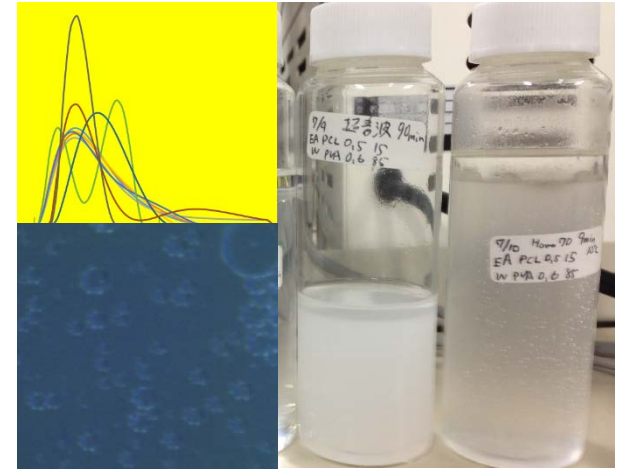
→→ L/G ratio calculation.



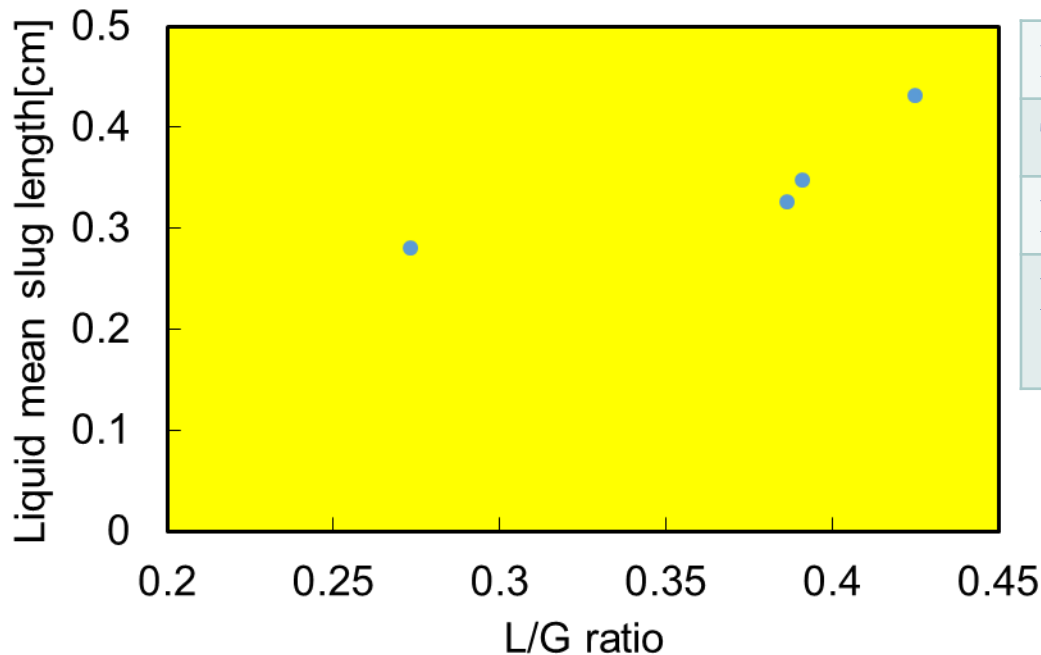
### 3. Results

- Main concerns – mean size & distribution.
- Instruments – homogenizer, ultrasonic washer, ultrasonic homogenizer (emulsion preparation), X-ray diffraction, digital microscope (diameter detection).
- Results – ultrasonic washer gives single-peak curve; *changed surfactant* stabilizes emulsion.

### \* Emulsion Preparation



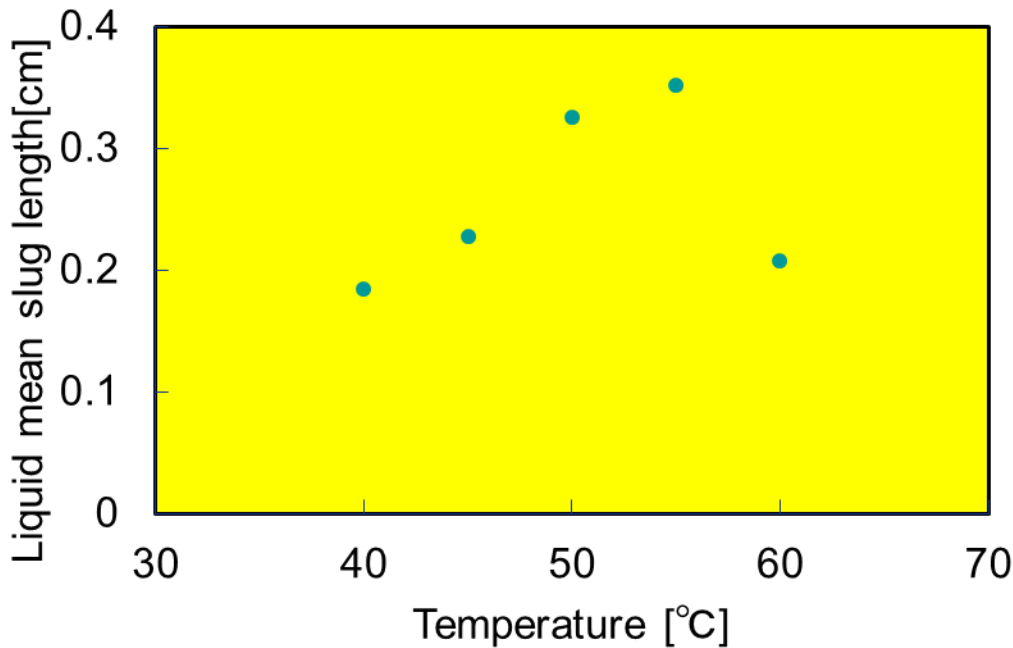
### Effect of L/G (Mass) Ratio



Pressure (Mpa)	8
Temperature (°C)	40
Needle Valve	0.10
Liquid Pump (mL/min)	0.25, 0.30, 0.35, 0.40

**Mean slug length increases with increasing L/G ratio.**

# Effect of Temperature



Pressure (Mpa)	8
Temperature (°C)	40, 45, 50, 55, 60
Needle Valve	0.05
Liquid Pump (mL/min)	0.30

**Mean slug length does not change monotonously with temperature.**

## Upward tendency

Decreased surface tension ( $\sigma$ ); ...

## Downward tendency

Increased volatility ( $P_S$ ) of liquid;

Decreased viscosity ( $\mu$ ) of liquid; ...

$$\frac{\langle L \rangle}{D} = \left( \frac{\mu_L^2}{\rho D^2 P_S} \right)^\alpha \left( \frac{\mu_L^2}{\rho D \sigma} \right)^\beta \left( \frac{\mu_L}{\mu_G} \right)^\gamma \left( \frac{L}{G} \right)^\delta$$

## ***Further study ...***

- Minimizing experimental error.
  - How operational parameters affect slug length. (simulation → real system)
  - How slug length affects the efficiency of the SEE process.
- ... → Insight into the mass transfer for new process design.

**~ Thanks for your attention ~**